

The following problems are based on the method of matched asymptotic expansions.

**Problem 1: Ordering breakdown**

Determine a two-term asymptotic solution for the equation

$$\frac{d^3 y}{dt^3} + \frac{d^2 y}{dt^2} + \epsilon \left[ \left( \frac{dy}{dx} \right)^2 + y \right] = \epsilon \exp(-2x) \quad (1)$$

on the unbounded domain  $x \geq 0$  and boundary conditions  $y(0) = 2$ ,  $\frac{dy}{dx}(0) = -1$  and  $\frac{d^2 y}{dx^2}(0) = 1$ . Where does ordering breakdown for the two-term expansion? What scaling do you expect for the ‘layer’ solution?

**Problem 2: Two term expansions**

Determine a two-term expansion for the following boundary value problem:

$$\epsilon \frac{d^2 y}{dx^2} + \sqrt{x} \frac{dy}{dx} + y^2 = 0 \quad x \in [0, 1] \quad (2)$$

subject to the boundary conditions  $y(0) = 2$  and  $y(1) = 1/3$  for  $\epsilon \rightarrow 0$ . Plot the numerical solution of this problem alongside the expansion you’ve determined above. Can you compute the maximum error inside the domain for  $\epsilon = 0.1$  and  $\epsilon = 0.001$ ?

**Problem 3: Multiple layers**

Consider the boundary value problem:

$$\epsilon \frac{d^4 y}{dx^4} - \left( \frac{1}{1 - \frac{3x}{4}} \right) \frac{dy}{dx} - 8 = 0 \quad x \in [0, 1] \quad (3)$$

subject to  $y(0) = \frac{dy}{dx}(0) = y(1) = \frac{dy}{dx}(1) = 0$ . Determine a composite expansion for  $y(x, \epsilon)$  as  $\epsilon \rightarrow 0$ . As in the previous question, compare your solution against a numerical evaluation for  $\epsilon = 0.1, 0.01$ .

**Problem 4: Turning layers**

For the equation

$$\epsilon^3 \frac{d^2 y}{dx^2} + (x - 2x^2)y = 0 \quad x \in [0, 1] \quad (4)$$

with boundary conditions  $y(0) = \alpha, y(1) = \beta$ , determine the location of transition layers and obtain the leading order term after matching.

**Problem 5: Laminar flow through a porous medium**

You are asked to evaluate the flow through a porous parallel plate channel of width  $2h$ . Assume that the Reynolds number is very high so that  $\epsilon = 1/Re \rightarrow 0$ .

- (a) Set up the problem assuming incompressible flow for a 2D flow field  $\vec{u} = (u(x, y), v(y))$  and boundary conditions  $u(x, y = \pm h) = 0$  and  $v(y = \pm h) = V_{\pm}$ . Assume that  $V_+ > V_-$ .

- (b) Using the continuity equation, determine  $u(x, y)$  and  $v(y)$  in terms of an unknown function  $u_0(x)$
- (c) From the Navier-Stokes equations for this configuration, obtain an expression for the kinematic pressure  $p(x, y) = \frac{1}{\rho}P(x, y)$ .
- (d) Non-dimensionalize all the equations, use  $V_+, h$  as velocity and length scales.
- (e) Derive a third order ODE for  $v(y)$  subject to the boundary conditions in part (a).
- (f) Solve for  $v(y)$  by evaluating possible combinations of values for  $V_{\pm}$ . Where does a layer occur in this problem?

If you are stuck, you might want to look at the reference: I Proudman, *J Fluid Mech*, 1960, where this problem was first presented.

### Problem 6: Heating of a current carrying insulated wire

Renovation of the department workshop has led to you questioning the need for large diameter (expensive) wires for high current applications. Consider a cylindrical wire of length  $L$  and radius  $R$  which has an outer insulation layer of thickness  $R_0 - R$ . The potential difference between the ends of the wire is  $V$ . Given that it has to carry large currents, the electrical  $\sigma$  and thermal  $K$  conductivities of the conducting part depend on temperature as:

$$\sigma = \sigma_0(1 - B(T - T_0)) \quad K = K_0(1 - A(T - T_0)) \quad (5)$$

the insulator layer has constant conductivity  $\kappa$ . The outer surface of the insulator cladding is maintained at temperature  $T_0$ , which also happens to be the reference temperature in Eq. 5.

- (a) Set up the problem using the heat conduction equation in both the core wire and the insulator. Remember that a volumetric heat source is operational inside the conducting part of the wire due to the current. Obtain an expression for this heat source.
- (b) What are the boundary conditions at  $r = R, r = R_0$ ?
- (c) Non-dimensionalize the entire system using  $\xi = r/R$  and  $\theta = (T - T_0)/T_0$ . The heating term should be now  $1/J$ . What is  $J$ ?
- (d) Solve the problem for very large  $J$  (what is the physical significance?) using dominant balance
- (e) Now solve the more difficult complementary problem for very small  $J \equiv \epsilon$ . Obtain two-term asymptotic expansion for  $T(r)$  in the core of the wire. Physically compare your results for  $J \gg 1$  and  $J \ll 1$ .

If you solved this problem in the year 1970, you could have published your result. For reference, you can find the solution to this problem in: Cohen and Shair, *Int J Heat Mass Transfer*, 1970.